

## Hydrous Ruthenium Oxide-Supported Pt and Pt-Ru Catalysts for the Oxidation of Methanol

Y. Murakami, Y. Izawa, T. Kawaguchi, W. Sugimoto,  
and Y. Takasu

Department of Fine Materials Engineering, Faculty of  
Textile Science and Technology, Shinshu University  
3-15-1 Tokida, Ueda 386-8567, JAPAN

Binary Pt-Ru/C is a promising CO-tolerant anode catalyst for use in direct-methanol fuel cells (DMFCs). The promotion effect has been mainly discussed based on so-called “bifunctional effect” [1] or “ligand effect” [2] or mixture of both. The bifunctional mechanism proposes that Ru promotes the oxidation of the strongly bound CO<sub>ad</sub> on Pt by supplying an oxygen source (Ru-OH<sub>ad</sub>). According to the ligand effect, the energy level of the catalyst is changed so that the binding strength of CO<sub>ad</sub> is weakened, thereby reducing the oxidation overpotential.

The actual state of the active ruthenium component is still a point of discussion. Some investigations suggest that hydrous ruthenium oxide is one of the active components for oxidation of the carbonaceous intermediates adsorbed on the catalyst surface in binary Pt-Ru black catalysts [3-5]. When Pt or Pt-Ru was deposited on hydrous ruthenium oxide, however, no significant electrochemical activity was found [6].

Pt/RuO<sub>2</sub>·xH<sub>2</sub>O catalysts were prepared by the liquid-phase reduction of H<sub>2</sub>PtCl<sub>6</sub>. H<sub>2</sub>PtCl<sub>6</sub> in an aqueous solution was completely reduced with 1-propanol at 87°C to Pt particles dispersed on commercial RuO<sub>2</sub>·xH<sub>2</sub>O ([Pt]:[RuO<sub>2</sub>·xH<sub>2</sub>O] = 3:7, 5:5 and 7:3).

Pt-Ru/RuO<sub>2</sub>·xH<sub>2</sub>O catalysts were prepared on the basis of a preparation method of Pt-Ru/C by Poizo et al. [7]. (NH<sub>3</sub>)<sub>2</sub>PtCl<sub>6</sub> and RuNO(NO<sub>3</sub>)<sub>x</sub> in an aqueous solution ([Pt]:[RuNO(NO<sub>3</sub>)<sub>x</sub>] = 1) were completely reduced with sodium borohydride at 110°C to Pt-Ru particles dispersed on commercial RuO<sub>2</sub>·xH<sub>2</sub>O ([Pt]:[Ru]:[RuO<sub>2</sub>·xH<sub>2</sub>O] = 1:1:8, 1:1:4, 1:1:2, 1:1:1, 2:2:1 and 4:4:1).

The working electrode was a thin film electrode composed of a mirror polished Glassy Carbon rod (0.196 cm<sup>2</sup> exposed surface) modified with 40 μg of the active material. A beaker-type electrochemical cell equipped with the working electrode, a platinum mesh counter electrode, and an Ag/AgCl reference electrode was used. Electrochemical measurements were conducted at 25°C. All electrode potentials will be referred to the RHE scale corrected for the temperature effect. Oxidation of pre-adsorbed carbon monoxide (CO<sub>ad</sub>) was measured by CO<sub>ad</sub> stripping voltammetry in 0.5 M H<sub>2</sub>SO<sub>4</sub> solution at a scan rate of 10 mV s<sup>-1</sup>. The electrochemical oxidation of methanol was characterized by the steady state current density at 0.5 V in 1 M CH<sub>3</sub>OH + 0.5 M H<sub>2</sub>SO<sub>4</sub> solution.

The CO<sub>ad</sub> stripping voltammograms were measured for Pt/RuO<sub>2</sub>·xH<sub>2</sub>O catalysts with various loadings. The CO<sub>ad</sub> oxidation potential for any Pt/RuO<sub>2</sub>·xH<sub>2</sub>O catalyst significantly decreased compared with that for the Pt/C catalyst. It suggests that no CO<sub>ad</sub> species was observed on RuO<sub>2</sub>·xH<sub>2</sub>O. These data support the bifunctional effect: RuO<sub>2</sub>·xH<sub>2</sub>O promotes the oxidation of the strongly bound CO<sub>ad</sub> on Pt by supplying an oxygen source.

Pt mass specific activities for the methanol oxidation were compared in Pt/RuO<sub>2</sub>·xH<sub>2</sub>O catalysts with

various loadings. The specific activities of Pt/RuO<sub>2</sub>·xH<sub>2</sub>O catalysts were independent of Pt-loadings and about 7 times as high as that of the Pt/C catalyst. No catalytic activity of RuO<sub>2</sub>·xH<sub>2</sub>O was observed for the methanol oxidation.

X-ray diffraction patterns of Pt-Ru/RuO<sub>2</sub>·xH<sub>2</sub>O catalysts were attributed to the face-centered cubic crystalline structure of Pt. The lattice parameter of the cubic phase was smaller than that of the Pt cubic phase. It suggests a fcc solid solution of Pt and Ru. The lattice parameter was reduced by the introduction of Ru in the Pt fcc structure.

The CO<sub>ad</sub> stripping voltammograms were measured for Pt-Ru/RuO<sub>2</sub>·xH<sub>2</sub>O catalysts with various loadings. The CO<sub>ad</sub> oxidation potential for any Pt-Ru/RuO<sub>2</sub>·xH<sub>2</sub>O catalyst significantly decreased compared with that for the Pt/C catalyst, similar to that for the Pt/RuO<sub>2</sub>·xH<sub>2</sub>O catalyst.

Pt mass specific activities for the methanol oxidation were compared in Pt-Ru/RuO<sub>2</sub>·xH<sub>2</sub>O catalysts with various loadings. The specific activities of Pt-Ru/RuO<sub>2</sub>·xH<sub>2</sub>O catalysts with high loadings ([Pt]/[RuO<sub>2</sub>·xH<sub>2</sub>O] = 2/1 and 4/1) were almost as high as that of the Pt/RuO<sub>2</sub>·xH<sub>2</sub>O catalyst, while, in the case of [Pt]/[RuO<sub>2</sub>·xH<sub>2</sub>O] = 1/4, the specific activity is about 3 times as high as that of the Pt/RuO<sub>2</sub>·xH<sub>2</sub>O catalyst. It suggests that binary Pt-Ru gives higher catalytic activity than Pt for highly dispersed Pt or Pt-Ru, while not highly dispersed Pt gives the similar activity to binary Pt-Ru because of the bifunctional effect of RuO<sub>2</sub>·xH<sub>2</sub>O.

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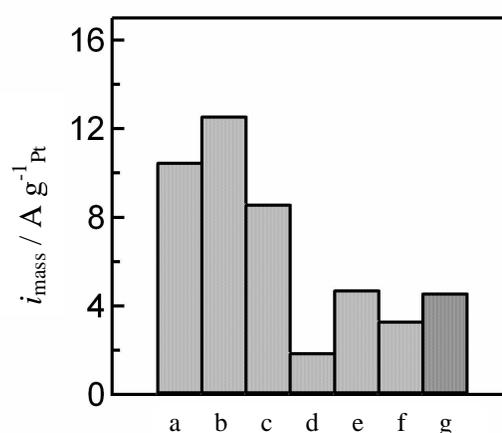


Figure 1 Pt mass specific activities of Pt-Ru/RuO<sub>2</sub>·xH<sub>2</sub>O with various loadings ([Pt]:[Ru]:[RuO<sub>2</sub>·xH<sub>2</sub>O] = (a) 1:1:8, (b) 1:1:4, (c) 1:1:2, (d) 1:1:1, (e) 2:2:1 and (f) 4:4:1) and (g) Pt/RuO<sub>2</sub>·xH<sub>2</sub>O ([Pt]:[RuO<sub>2</sub>·xH<sub>2</sub>O] = 1:1) for the methanol oxidation at 0.5 V in 1 M CH<sub>3</sub>OH + 0.5 M H<sub>2</sub>SO<sub>4</sub> solution.